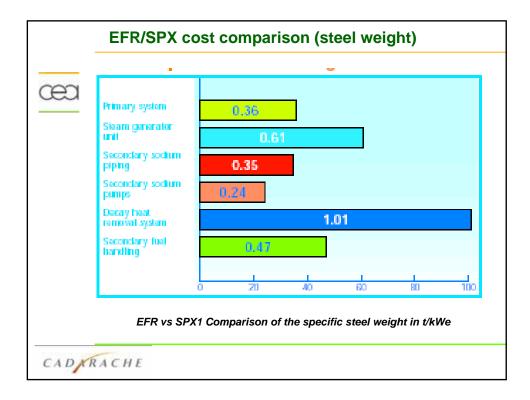
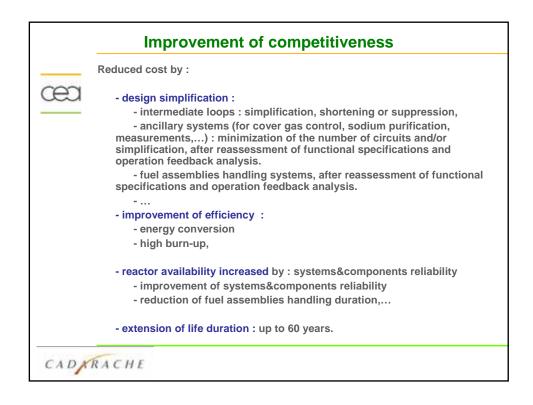
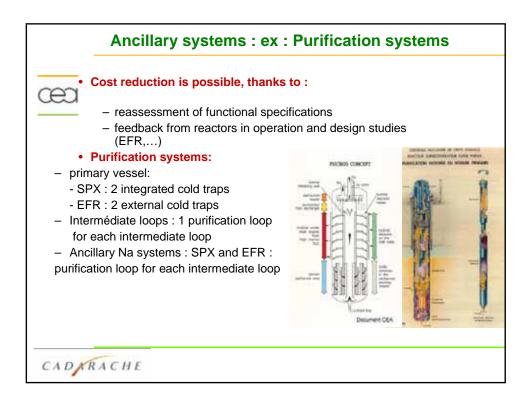


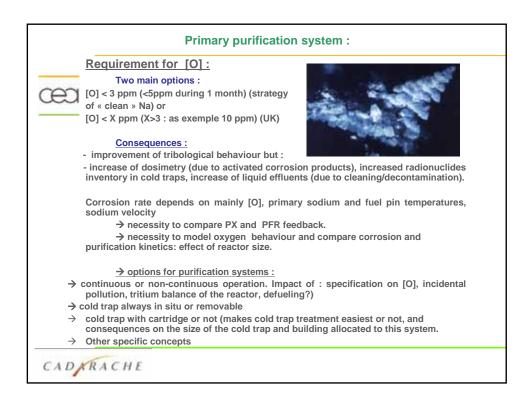
	Improvement of safety:		
ඥා	Reactor designed in order to reduce strongly the probability of core melting; nevertheless a reference accident involving a core melting event will be postulated, investigated and demonstrated as mastered.		
-	Protection against plane shut-down,		
-	Elimination of environmental consequences outside the nuclear plant ; necessity to focus on incidents involving Na, (sodium leaks, release) :		
	<ul> <li>Sodium pipes and/or systems inertization</li> <li>Sodium leak control systems : reliability improvement</li> </ul>		
	<ul> <li>Optimized In Service Inspection strategy</li> </ul>		
	<ul> <li>Efficient, safe and fast Repair operations.</li> <li>Minimization of Liquid&amp;gaseous effluent releases (« zero » release?),</li> </ul>		
CANNO DO			
CADAR	ACHE		

On site workshop	2,7
Reactor assembly structures	19,4
secondary handling	5,7
secondary circuit	9,0
DRACS	3,7
SGU	11,0
primary auxiliary system	48,6
	100,0

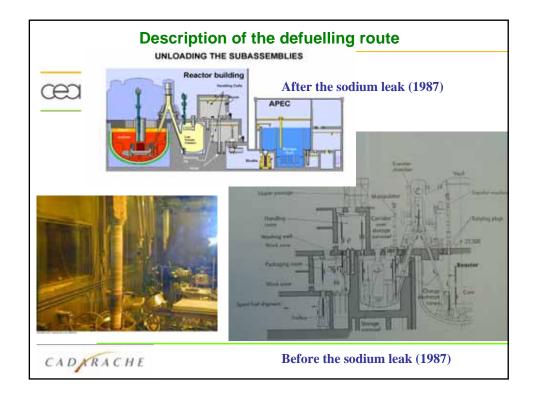


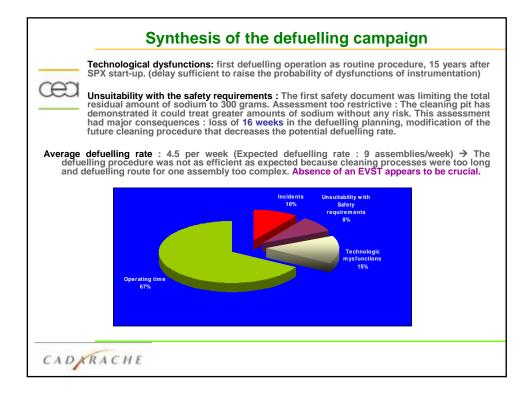


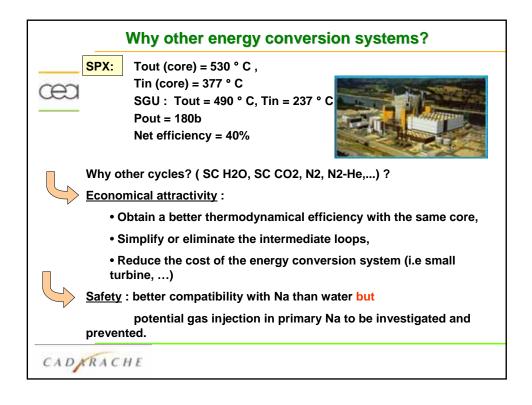


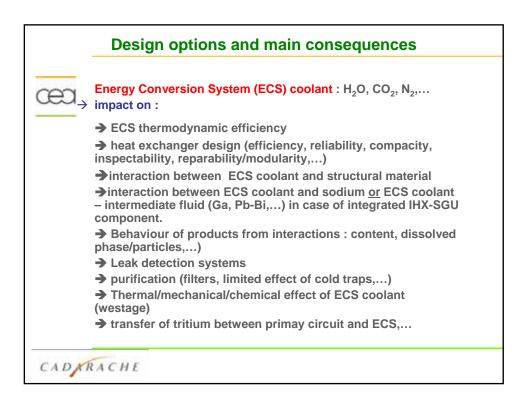


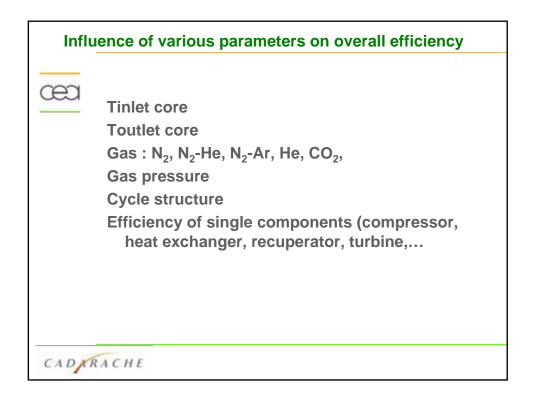
	Case : Rankine Cycle (H <sub>2</sub> O):
and the sould be	Specifications on :
œ	- nominal residual [H] : with regards to efficient fast water-sodium detection in SGU
	- tritium release (EFR : difficulty to fulfill requirements due to choice of ferritic steel Steam Generator : aqueous corrosion increased→ continuous H source increased)
	$\rightarrow$ H trapping in intermediate cold traps allows to trap also tritium and to control release.
	- incidental purification campaign : anticipated Na2O and NaH inventory.
	→ options for purification systems :
	$\rightarrow$ continuous or non-continuous operation ? Impact of : specification on [H], incidental pollution, tritium balance of the reactor, )
	ightarrow cold trap always in situ or removable
	→ cold trap able to be regenerated or not, with cartridge or not (makes cold trap treatment easiest or not, and consequences on the size of the cold trap and building allocated to this system.
	→ cold trap for continuous and incidental pollution or not (specific removable cold trap for incidental pollution, able to be installed on the involved loop)
	→ other concepts?

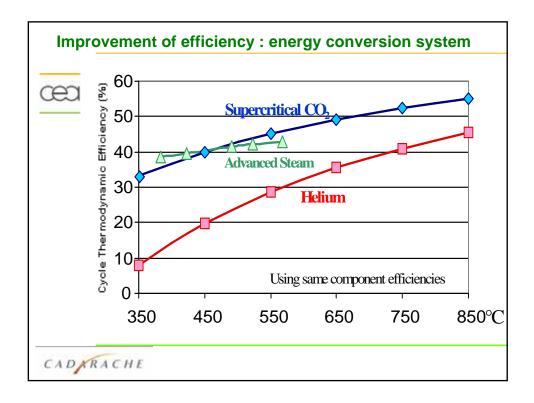


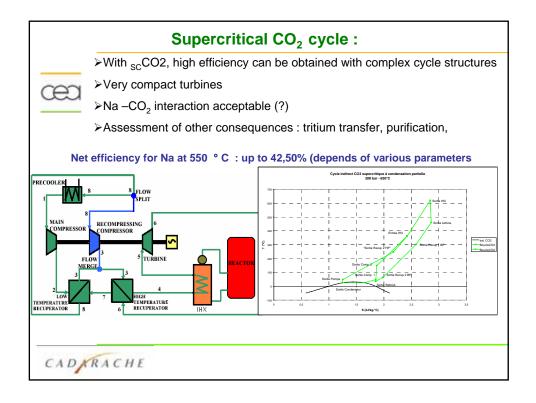


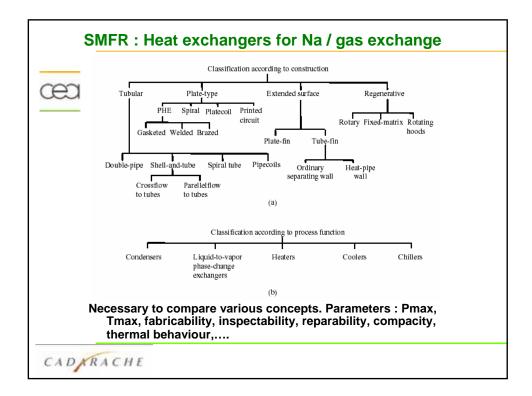


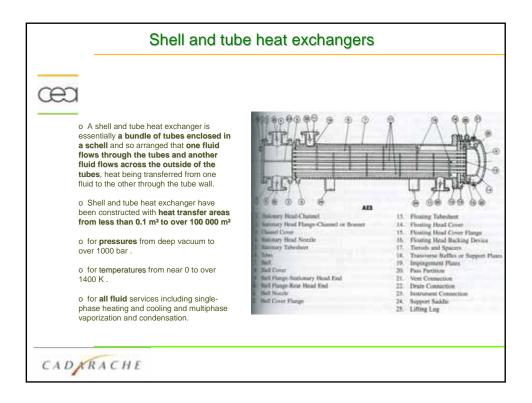


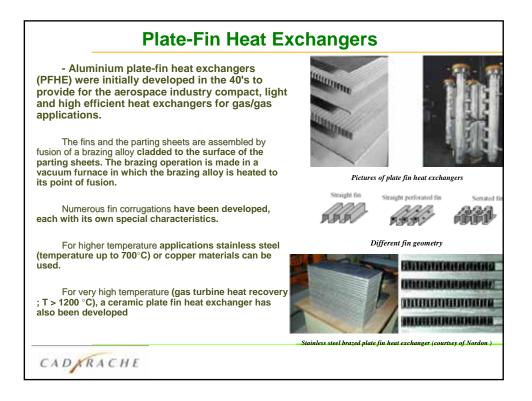


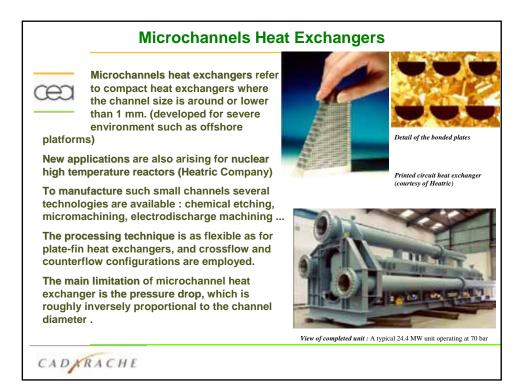


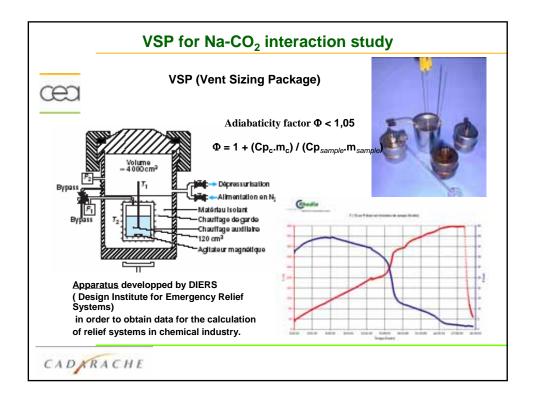


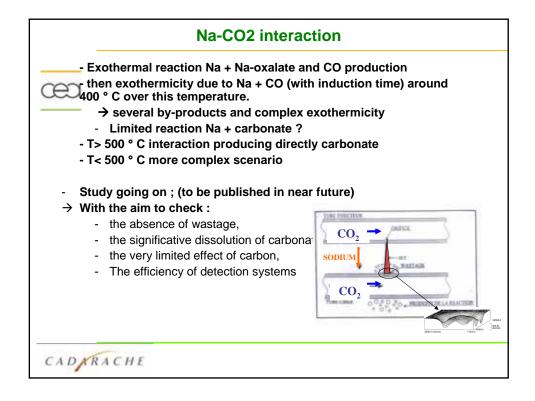






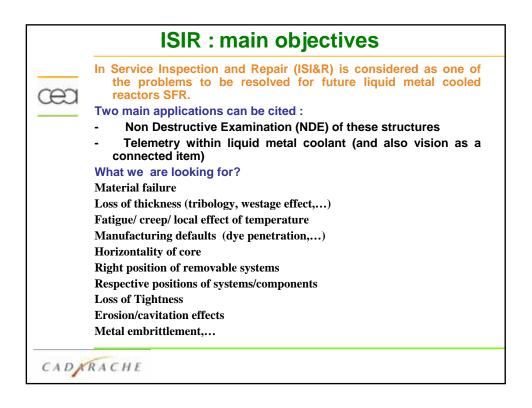


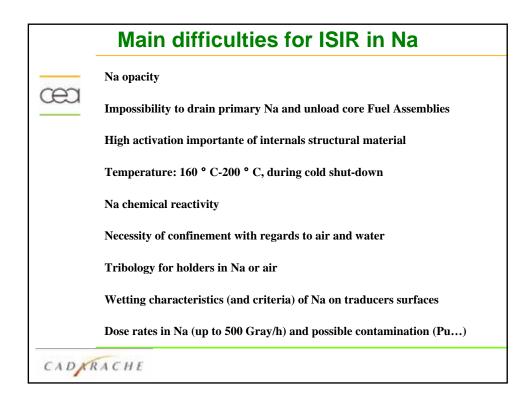


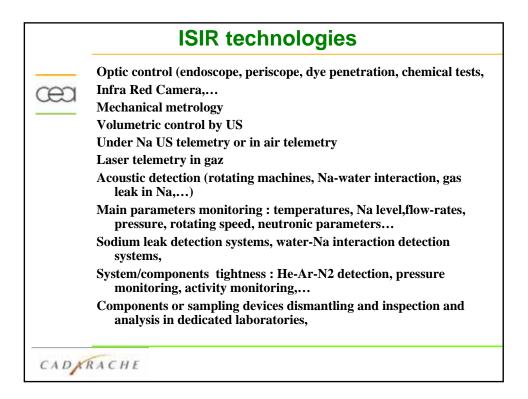


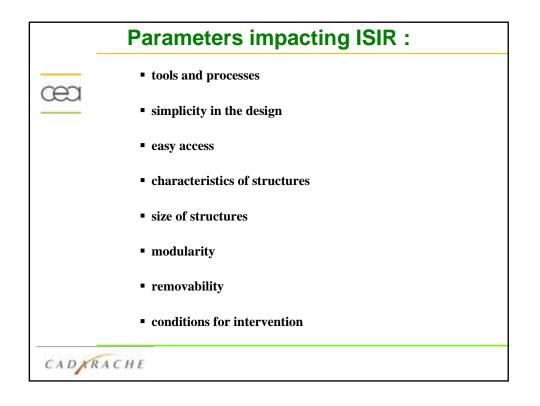
Comparison Na-CO <sub>2</sub> , Na-H <sub>2</sub> O (1/2)						
Event	Water ingress	CO <sub>2</sub> ingress	Comments			
Pressure (H <sub>2</sub> O or CO <sub>2</sub> )	168 bar	200 bar	Impact of pressure on heat exchanger design			
ΔH (kJ/mol)	162	271.5				
Kinetics of reaction	Almost instantaneous	Order 2 / CO <sub>2</sub>	For CO <sub>2</sub> to be investigated in realistic conditions			
Products of reaction	NaOH, O <sup>=</sup> , H <sup>-</sup>	Na <sub>2</sub> CO <sub>3</sub> , C, and Na <sub>2</sub> C <sub>2</sub> , Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub> as intermediate products	Necessity to investigate carbonate dissolution in sodium			
Particulates?	Not	Yes (Na <sub>2</sub> CO <sub>3</sub> )	Necessity to foresee filters			
Soluble products trapping	Cold trap, hot trap	To be defined	Necessity to foresee a carbon trap?			
Non soluble products trapping	Not necessary	Filters,	Implementation has to deal with thermo-hydraulics			

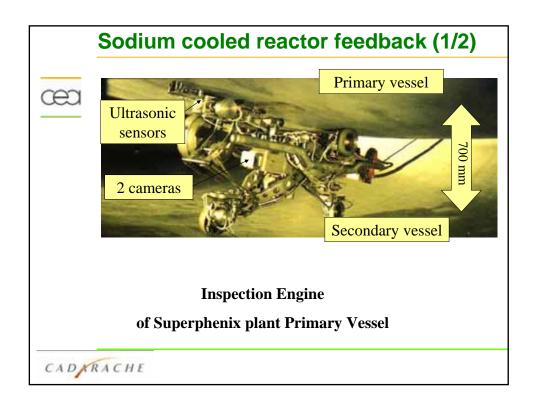
Comparison Na-CO <sub>2</sub> , Na-H <sub>2</sub> O (2/2)						
General corrosion	Yes but very limited due to NaOH conversion with Na	Not				
Carburization	No	Yes at high temperature and high C content	Probably very limited consequences			
Possibility of Leak detection	Yes (hydrogen-meter, acoustic detection system,)	Yes (diffusion or electrochemical carbon meter, sampling then analysis,)	Necessity to assess the response time for CO <sub>2</sub>			
Wastage	Yes	Probably not	To be investigated			
Risk of strong reaction	Yes, if contact with oxygen	Not	Probability of loss of tightness of gas plenum to be investigated			
Risk of combustion	Not	Yes	Operating conditions to be investigated			

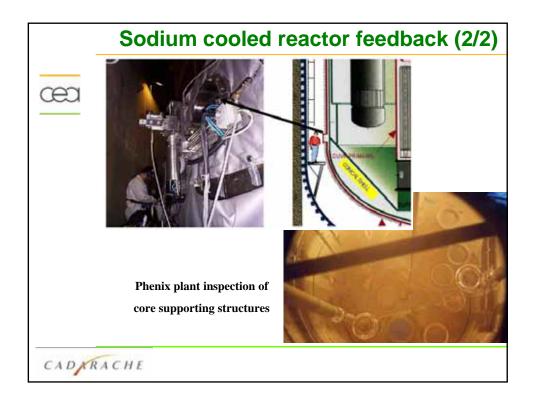


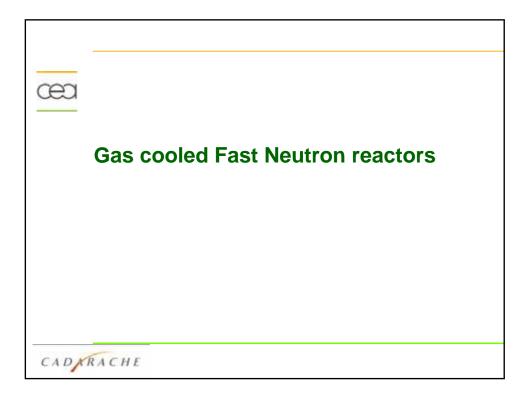


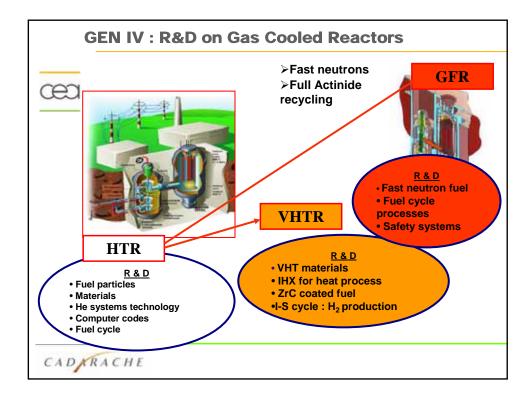


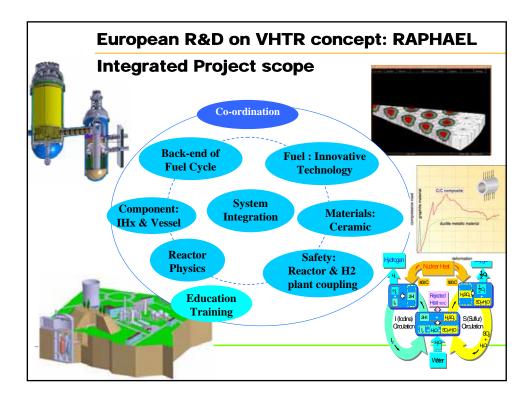


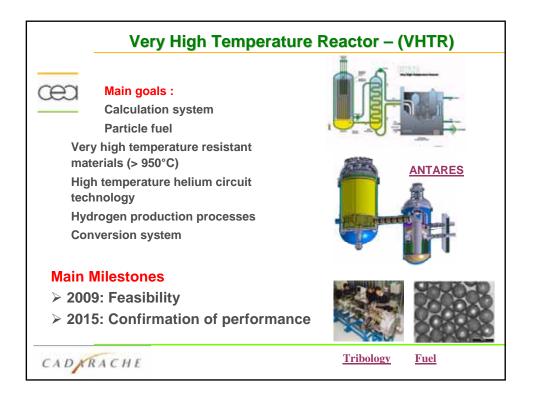


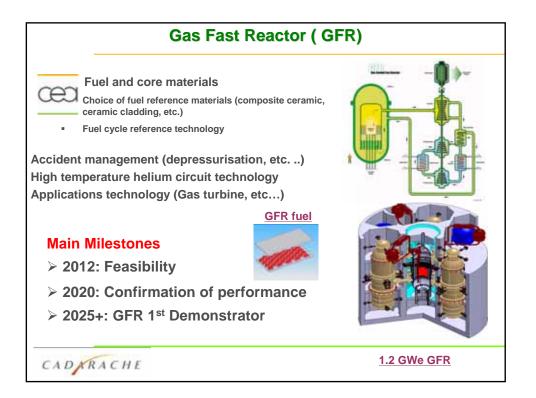




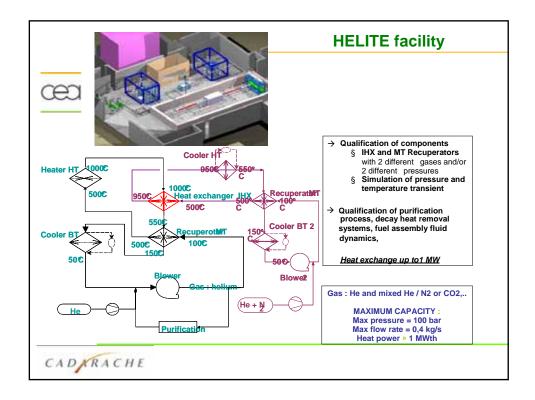


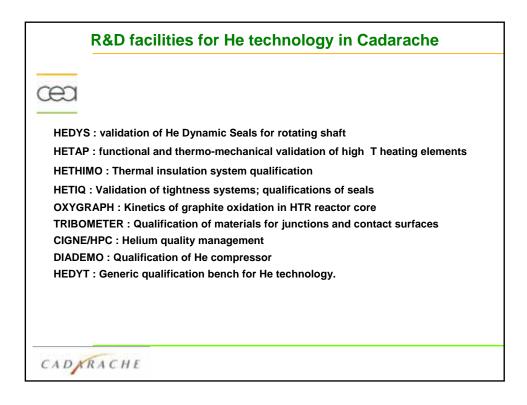


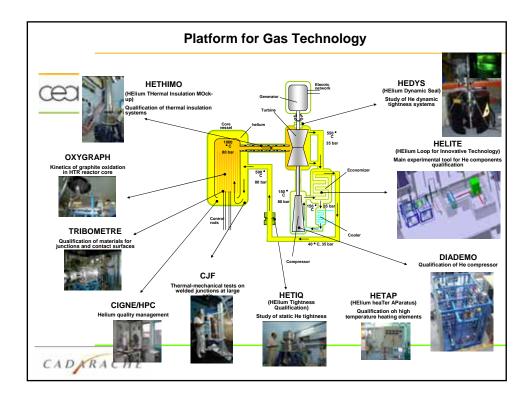


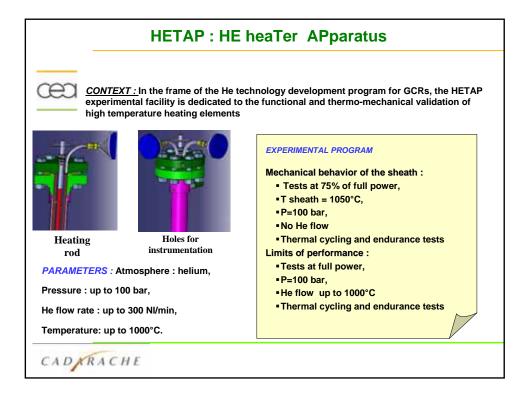


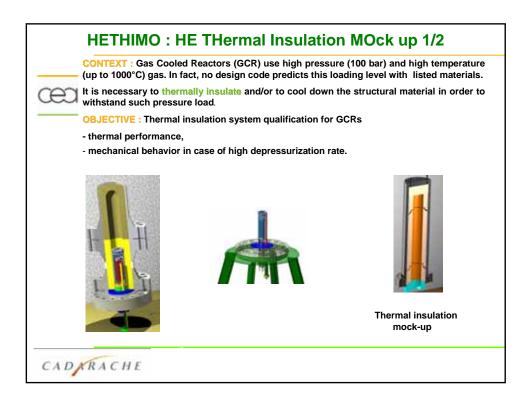


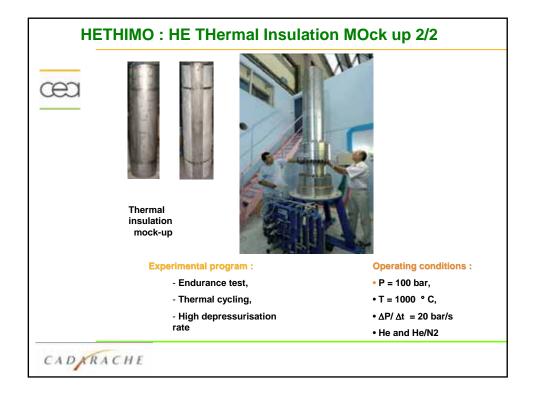


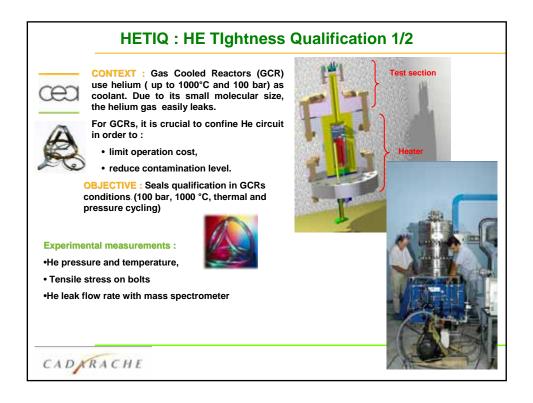


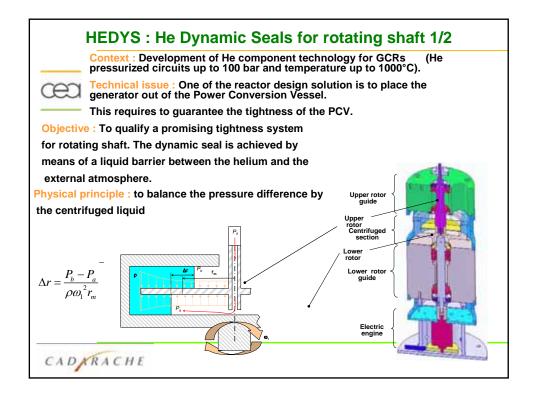


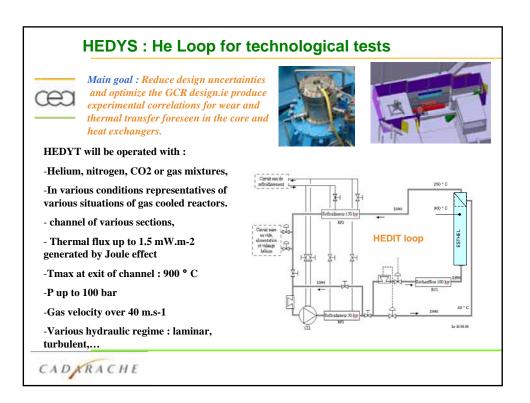


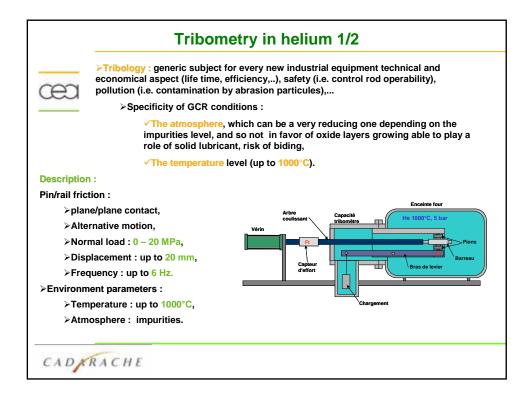


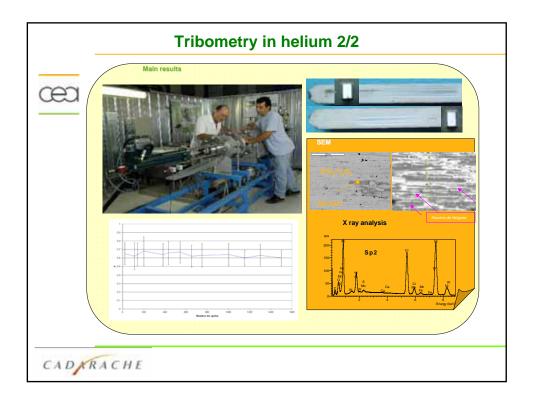


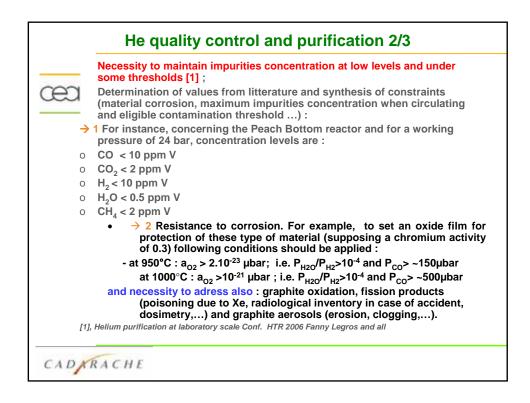


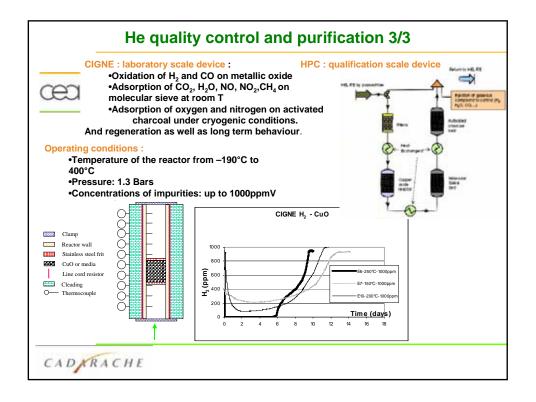


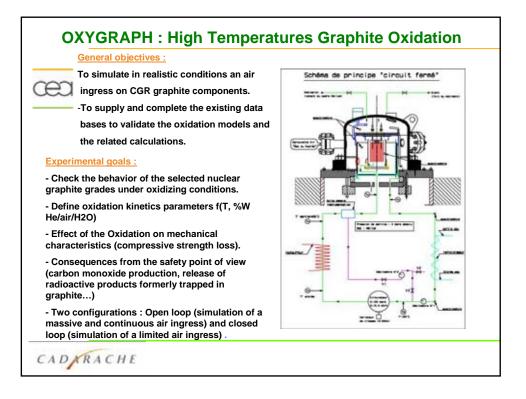




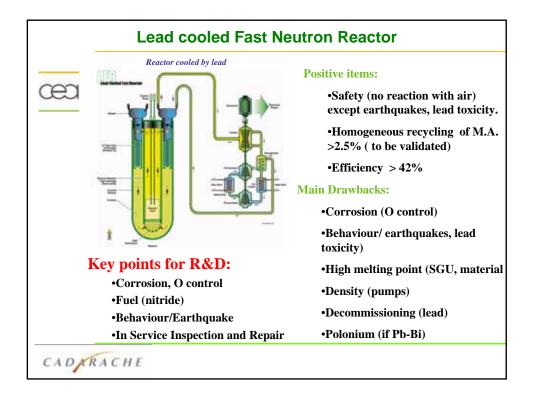




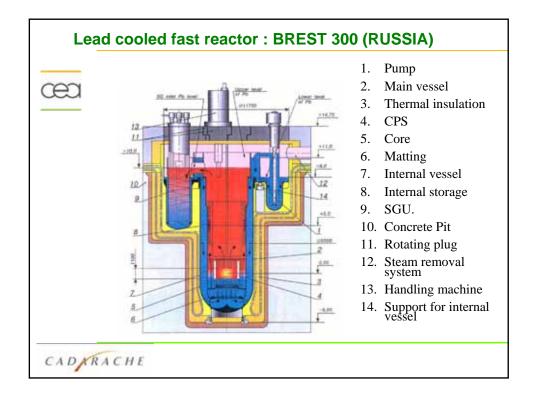


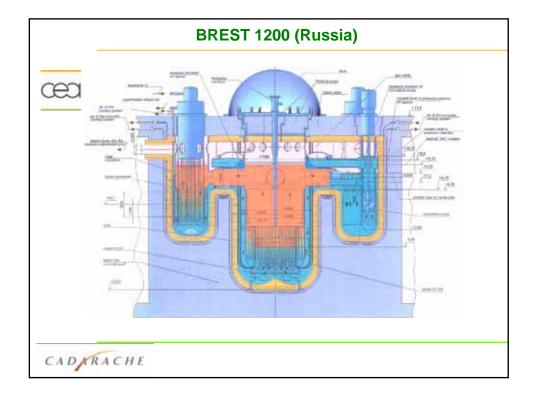


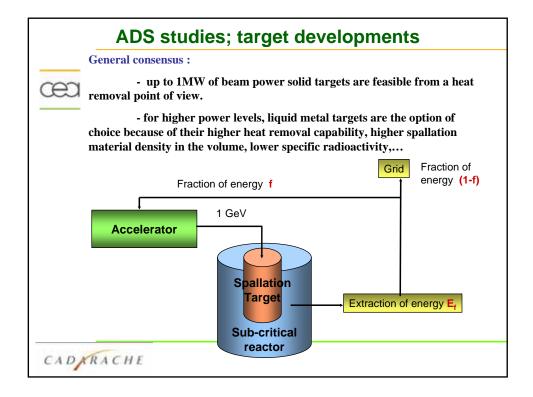


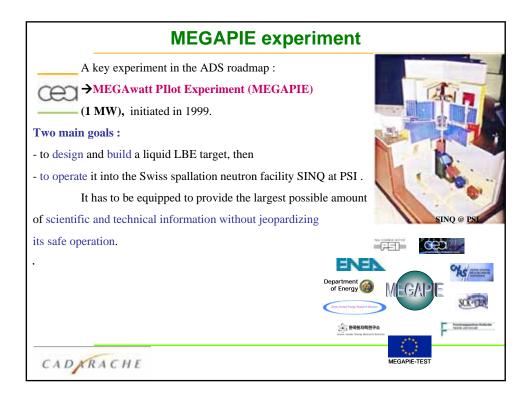


$\sim$							
r	Property		Pb	Bi	LME *	LBE**	Hg
	Composition		elem.	elem.	Pb 97.5% Mg 2.5%	Pb 45% Bi 55%	elem.
	Atomic mass A (g/mole)		207.2	209	202.6	208.2	200.6
	Density	20°C	11.35	9.75			10.5
	(g/cm <sup>3</sup> )	liquid	10.7	10.07	10.6	10.5	13.55
	Linear coefficient of	solid	2.91	1.75			
	thermal expansion (10 <sup>-5</sup> K <sup>-1</sup> )	liquid (400°C)	4		4		6.1
	Volume change upon solidification (%)		3.32	-3.35	3.3	0	
	Melting point (°C)		327.5	271.3	250	125	-38.87
	Boiling point at 1 atm (°C)		1740	1560			356.58
	Specific heat (J/gK)		0.14	0.15	0.15	0.15	0.12
	Thermal neutron absorption (barn)		0.17	0.034	0.17	0.11	389
·		c ** LBE - lea	d/bismuth	eutectic			

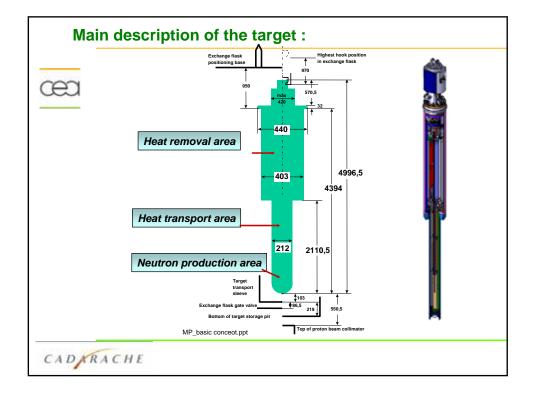


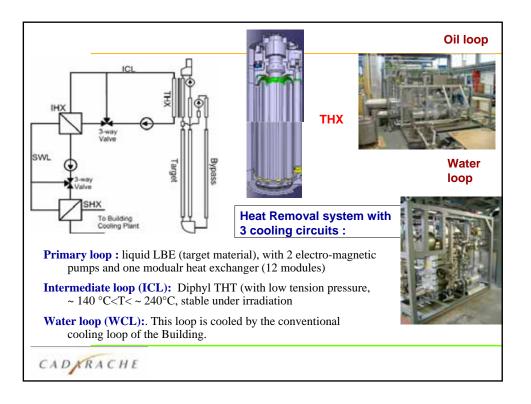


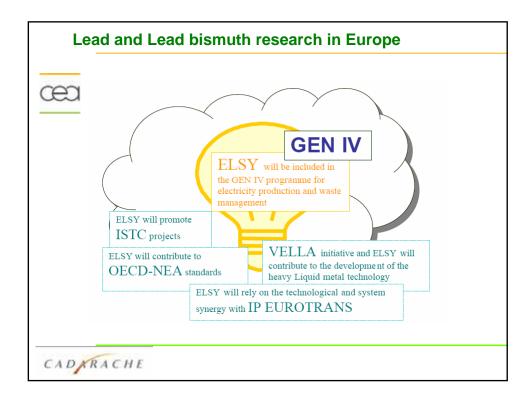


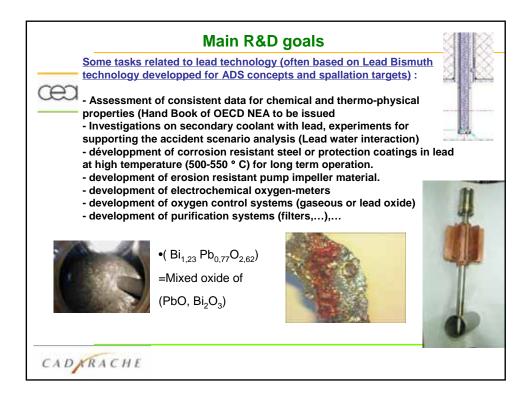


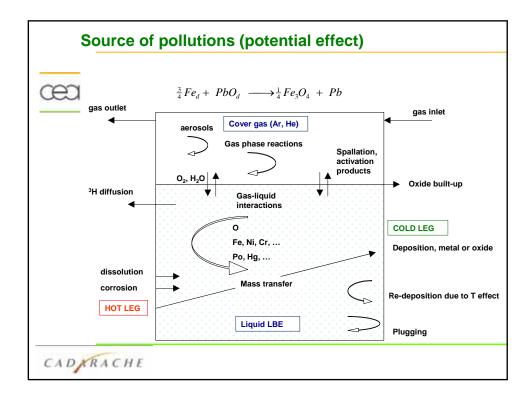
a	Lead bismuth eutectic neutronic and physica (125 ° C); nevertheless bismuth polonium,	al properties :	heat tran	sfer coe	fficient, lo	ow melti	ng poi
	Property		Pb	Bi	LME *	LBE**	Hg
	Composition		elem.	elem.	Pb 97.5% Mg 2.5%	Pb 45% Bi 55%	elem.
	Atomic mass A (g/mole)		207.2	209	202.6	208.2	200.6
	Density	20°C	11.35	9.75			10.5
	(g/cm <sup>3</sup> )	liquid	10.7	10.07	10.6	10.5	13.55
	Linear coefficient of	solid	2.91	1.75			
t	hermal expansion (10 <sup>-5</sup> K <sup>-1</sup> )	liquid (400°C)	4		4		6.1
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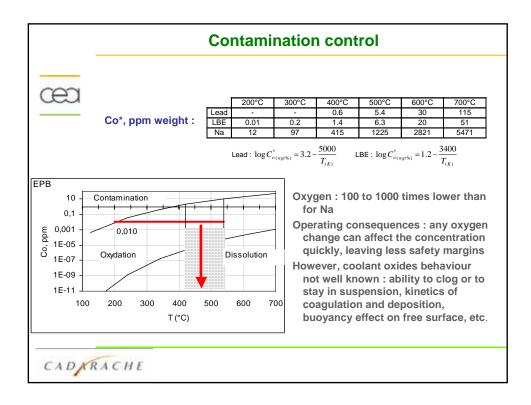


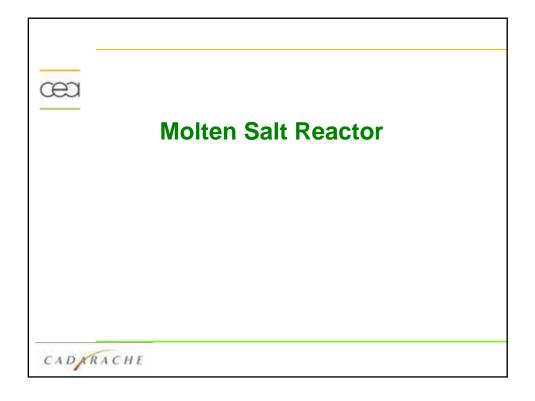


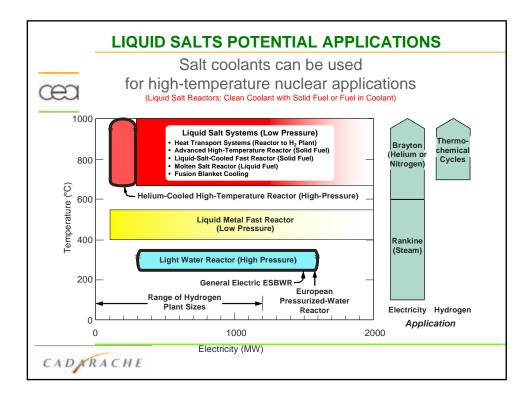


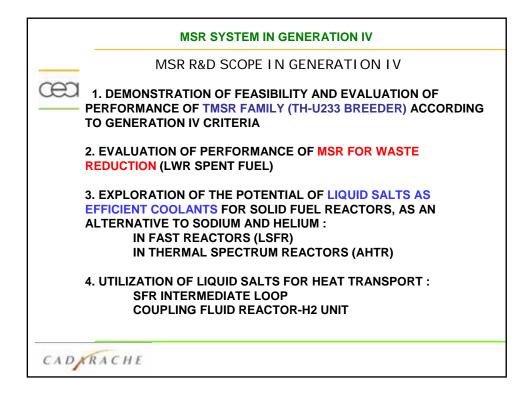


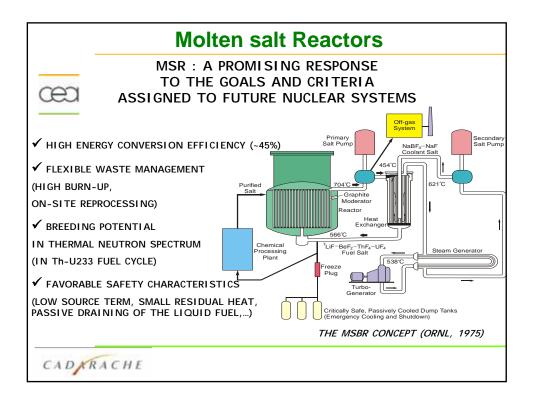


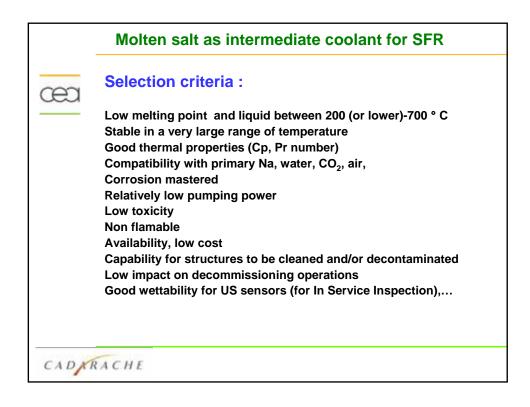












LIQUID SAL	TS POTEN				nts		
		helium	CO <sub>2</sub>	water	sodium	FLiBe	
	unit	60 bar 500°C	60 bar 500°C	150 bar 300°C	1 bar 500°C	T > 450°C	
ρ	kg/m <sup>3</sup>	3.7	40.9	726	865	1940	
Cp	kJ/kg.K	5.2	1.2	5.6	1.3	2.3	
ρc <sub>p</sub>	kJ/m <sup>3</sup> .K	19.4	48.6	4066	1125	4540	
λ	W/m.K	0.29	0.06	0.56	80	1.0	
μ	10 <sup>-5</sup> *Pa/s	3.8	3.3	9.0	23.3	563	
Pr	-	0.67	0.66	0.90	0.004	13.2	
relative merit* (ref. Na)	-	0.001	0.003	51	1	14	5
*merit factor =	$c_{p}^{2,8}\rho^{2}\mu^{-0,2}$						
Good compatibility wit	h water , ai	r,Non fl	amable,	low toxici	ty, low co	ost,	
CADARACHE							

Some other examples of salts :									
Œ	20								
	Sel	Composition	Tfusion	Tmax	Density at 300 ° C	Used for solar plants			
	Hitec	7%NaNO <sub>3</sub> 40%NaNO <sub>2</sub> 53%KNO <sub>3</sub>	142 ° C	535 ° C	1,6	THEMIS (2,5MWe)			
	Drawsalt	46%- 60%NaNO <sub>3</sub> 54%- 40%KNO <sub>3</sub>	220 ° C	600 ° C	1,9	SOLAR 2 (10MWe)			
		Salts at low mel teria previously			compa	red /			
C	DARACI	H E							

